

Ch 2 Equation of State

2.1 Introduction

In thermodynamics, 在原有 mass, length, time 3個基本量外, 又加上一個基本量 temperature.

The concept of temperature 源自於 systems in thermal equilibrium.

Simplest thermodynamic system perhaps is a homogeneous fluid - say, a gas or vapor.

$$\boxed{P, V, T} \quad f(P, V, T) = 0.$$

Three state variables, only two are independent.

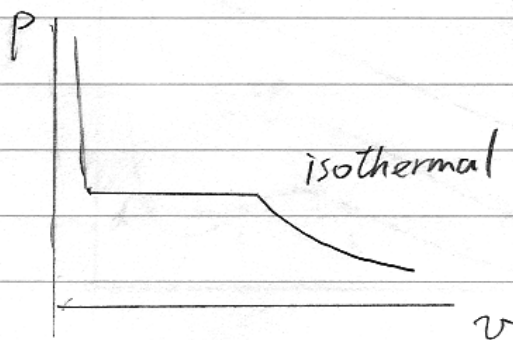
注意 The equation of state does not involve time. Systems are in thermal, mechanical, and chemical equilibrium that is thermodynamic equilibrium.

Canonically conjugate pairs: extensive 與 intensive 成對
且乘積為能量
 $PdV = W.$

T 的對應量將在 ch 6 中討論.

2.3 Van der Waal's Equation for a Real Gas

When the gas is near condensation, equation of state of an ideal gas 不適用。



很多 equations of state 被提出來敘述此 real gas 現象
在此介紹 Van der Waal's eq. of state.
因它簡單, ②有物理意義. ③適用於很大的溫度, 壓力範圍.

$$\left(P + \frac{a}{v^2}\right)(v-b) = RT \quad (2.5)$$

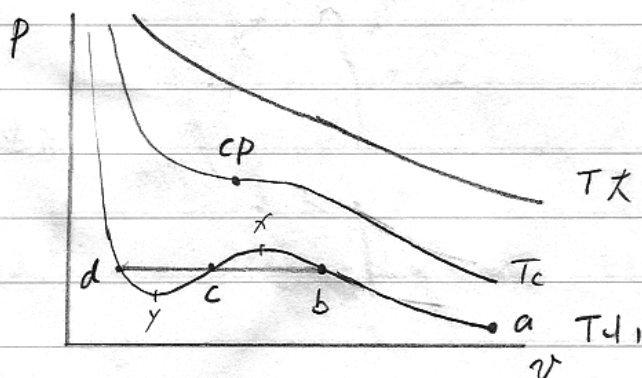
a 及 b 是特性常數, 隨氣體本質而定。

[b 反應氣體分子實際佔有的體積。

[a 反應氣體分子間的交互作用力 cohesive force.
來自於 the overlap of electron clouds.

(2.5) 乘開為： $Pv^3 - (Pb + RT)v^2 + av - ab = 0$ (2.6)

Isothermal process: P 是 v 的 3 次方程式，其解如下：



$T \rightarrow$ 大：行為近似理想氣體。

$T = T_c$ ：有一個水平點，稱作 critical point CP，此線為 critical curve.

$T < T_c$ ：有二個水平點，此類曲線並不合理。

在 x 與 y 間 P, v 同時增大或減小，顯然不符現實。

實際上 $a \rightarrow b$ 是 vapor, $b \rightarrow d$ 的水平直線是液氣共存。

d 以下完全液化。

2.4 P-v-T surfaces for Real Substances

P25, Fig 2.3: 實際物質的 state surface in P-v-T space.
水的不一樣。

注意固、液、氣三種 phases 的區域。

注意 triple line, where all three phases can coexist.

物理定義: solid: 體積, 形狀固定

Liquid: 體積固定, 形狀不定

Gas: 體積, 形狀均不固定, 加壓不液化。

Vapor: 等溫線低於 critical curve, 加壓會液化者

沸點: boiling-point, saturated vapor.

水燒開時, 飽和蒸氣壓 = 外界大氣壓, why?

P26, Fig 2.4: 觀察三相變化及邊界。

液氣間, 溫度或壓力高於 CP 時, 液氣不分。

固、液相變無臨界點, 因兩種相的對稱性不同。

P26 - P27: 舉例。

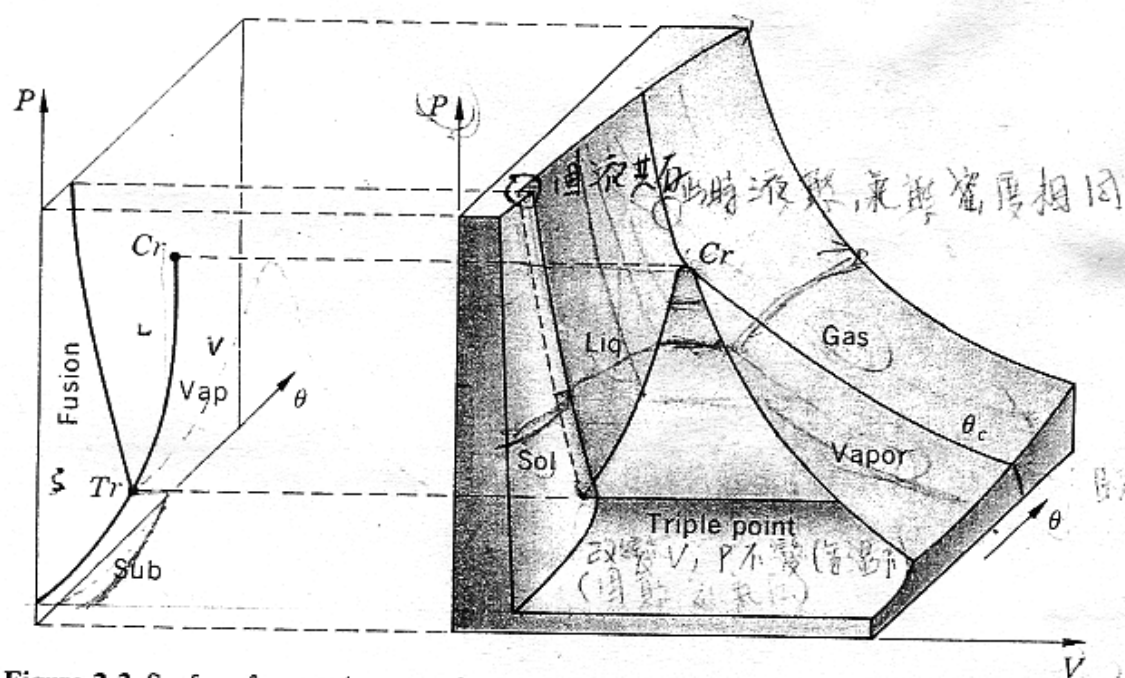


Figure 2-3 Surface for a substance that contracts on melting.

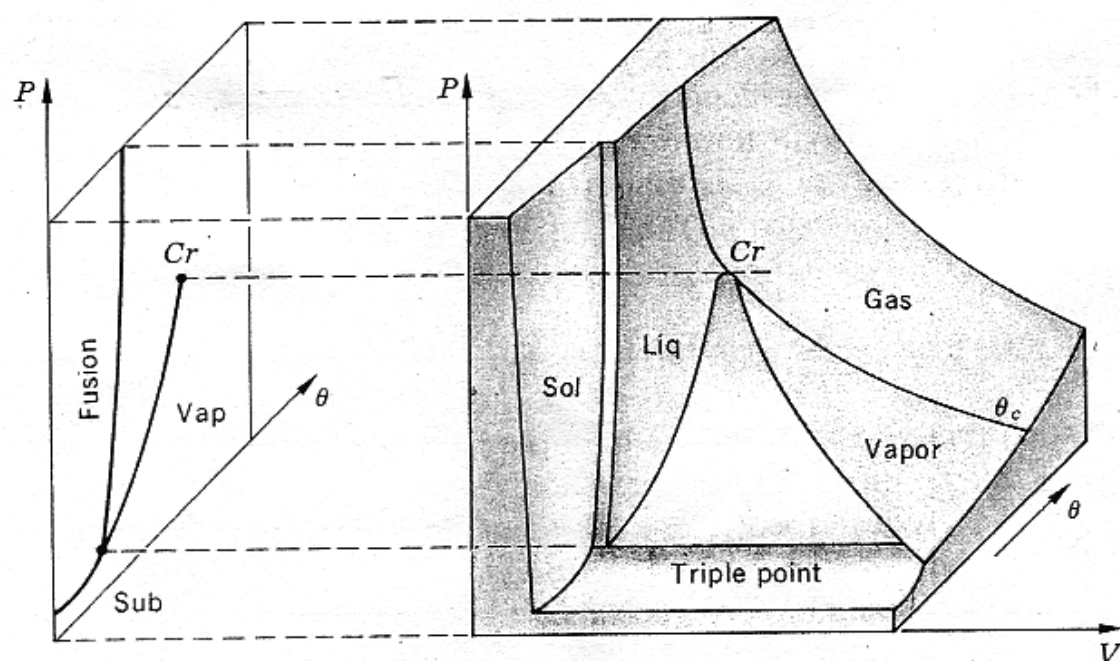


Figure 2-4 Surface for a substance that expands on melting.

2.5 Expansivity and Compressibility

P, V, T

System : state variables P, v, T , 獨立變數 2 個.

equation of state:

$$v = v(T, P)$$

$$\Rightarrow dv = \underbrace{\left(\frac{\partial v}{\partial T}\right)_P}_{\text{定義 } v\beta} dT + \underbrace{\left(\frac{\partial v}{\partial P}\right)_T}_{-v\kappa} dP$$

定義 $v\beta$ $-v\kappa$

$\beta \equiv \frac{1}{v} \left(\frac{\partial v}{\partial T}\right)_P$: expansivity or coefficient of volume expansion

$\kappa \equiv \frac{-1}{v} \left(\frac{\partial v}{\partial P}\right)_T$: isothermal compressibility.

↑
因 $\left(\frac{\partial v}{\partial P}\right)_T < 0$, 故加 "-" 使 $\kappa > 0$.

$$\text{For ideal gas } v = \frac{RT}{P} \Rightarrow \begin{cases} \beta = \frac{R}{Pv} = \frac{1}{T} \\ \kappa = \frac{-1}{v} \left(\frac{-RT}{P^2}\right) = \frac{1}{P} \end{cases}$$

\Rightarrow 高溫氣體 β 很小, 高壓氣體 κ 很小。

For a liquid or a solid, β and κ are near constant over a wide range of T and P .

$$\Rightarrow dv = \beta v dT - \kappa v dP$$

因 v 變化極小, 可視為常數 $\Rightarrow dv \approx \beta v_0 dT - \kappa v_0 dP$.

因 v_0, β, κ 均是常數 (固, 液)

$$\int_{v_0}^v dv = \beta v_0 \int_{T_0}^T dT - \kappa v_0 \int_{P_0}^P dP$$

$$\Rightarrow v = v_0 \left[1 + \beta(T - T_0) - \kappa(P - P_0) \right]$$

固液體的近似方程式, v 與 T, P 的變化呈線性關係。

Appendix A

A1 Partial Derivatives

x, y, z 3個變數, 有一個關係式: $f(x, y, z) = 0$.

可任取 2 個為獨立變數, $\Rightarrow \begin{cases} x(x, z) \\ y(x, z) \end{cases}$

$$\Rightarrow dx = \left(\frac{\partial x}{\partial y} \right)_z dy + \left(\frac{\partial x}{\partial z} \right)_y dz \quad \text{--- (A2)}$$

$$dy = \left(\frac{\partial y}{\partial x} \right)_z dx + \left(\frac{\partial y}{\partial z} \right)_x dz \quad \text{--- (A3)}$$

$$(A3) \text{ 代入 } (A2) \Rightarrow dx = \left(\frac{\partial x}{\partial y} \right)_z \left[\left(\frac{\partial y}{\partial x} \right)_z dx + \left(\frac{\partial y}{\partial z} \right)_x dz \right] + \left(\frac{\partial x}{\partial z} \right)_y dz$$

$$\Rightarrow dx = \left(\frac{\partial x}{\partial y} \right)_z \left(\frac{\partial y}{\partial x} \right)_z dx + \left(\frac{\partial x}{\partial y} \right)_z \left(\frac{\partial y}{\partial z} \right)_x dz + \left(\frac{\partial x}{\partial z} \right)_y dz \quad \text{(A4)}$$

因有2個獨立變數，取 x, z .

$$\text{若 } dz = 0 \Rightarrow \left(\frac{\partial x}{\partial y}\right)_z \left(\frac{\partial y}{\partial x}\right)_z = 1 \quad (\text{A.5})$$

$$\text{若 } dx = 0 \Rightarrow \left(\frac{\partial x}{\partial y}\right)_z \left(\frac{\partial y}{\partial z}\right)_x = -\left(\frac{\partial x}{\partial z}\right)_y \quad (\text{A.6})$$

$$(\text{A.5}) \Rightarrow \left(\frac{\partial x}{\partial y}\right)_z = \frac{1}{\left(\frac{\partial y}{\partial x}\right)_z} \Rightarrow \boxed{\left(\frac{\partial x}{\partial z}\right)_y = \frac{1}{\left(\frac{\partial z}{\partial x}\right)_y}} \quad \text{reciprocal relation}$$

$$\text{再代入 (A.6)} \Rightarrow \left(\frac{\partial x}{\partial y}\right)_z \left(\frac{\partial y}{\partial z}\right)_x = \frac{-1}{\left(\frac{\partial z}{\partial x}\right)_y}$$

$$\Rightarrow \boxed{\left(\frac{\partial x}{\partial y}\right)_z \left(\frac{\partial y}{\partial z}\right)_x \left(\frac{\partial z}{\partial x}\right)_y = -1} \quad (\text{A.7})$$

cyclical rule
cyclical relation

$$\text{show chain rule } \left(\frac{\partial x}{\partial z}\right)_u = \left(\frac{\partial x}{\partial y}\right)_u \left(\frac{\partial y}{\partial z}\right)_u \quad (\text{A.11})$$

system 有變數 x, y, z, u ，獨立變數2個 (可任取，有6種取法)

$$\Rightarrow \begin{bmatrix} u(x, y), & x(u, y), & \dots \\ z(x, y), & z(u, y), & \dots \end{bmatrix}$$

$$\text{由 } x = x(u, y) \Rightarrow dx = \left(\frac{\partial x}{\partial u}\right)_y du + \left(\frac{\partial x}{\partial y}\right)_u dy$$

$$\text{使 } u \text{ 不變，將 } dx \text{ 除以 } dz \Rightarrow \left(\frac{\partial x}{\partial z}\right)_z = \left(\frac{\partial x}{\partial y}\right)_u \left(\frac{\partial y}{\partial z}\right)_u$$

2.6 An Application

計算^{fluid}流体溫度由 T_1 cool down to T_2 時壓力變化 ($T_2 < T_1$)

system P, v, T , 2 個獨立變數。
 $f(P, v, T) = 0$.

設 cooling process 是 quasi-static process, 是 reversible, 是 Isochoric, 每步都是平衡態。

$$\Rightarrow P = P(v, T)$$

$$\Rightarrow dP = \left(\frac{\partial P}{\partial v}\right)_T dv + \left(\frac{\partial P}{\partial T}\right)_v dT$$

\downarrow because it is isochoric

$$\Rightarrow \int_{P_1}^{P_2} dP = \int_{T_1}^{T_2} \left(\frac{\partial P}{\partial T}\right)_v dT$$

$$\begin{aligned} \text{因 } \left(\frac{\partial P}{\partial T}\right)_v \left(\frac{\partial T}{\partial v}\right)_P \left(\frac{\partial v}{\partial P}\right)_T &= -1 \\ \Rightarrow \left(\frac{\partial P}{\partial T}\right)_v &= \frac{-1}{\left(\frac{\partial T}{\partial v}\right)_P \left(\frac{\partial v}{\partial P}\right)_T} = \frac{-\left(\frac{\partial v}{\partial T}\right)_P}{\left(\frac{\partial v}{\partial P}\right)_T} = \frac{\beta}{\kappa} \end{aligned}$$

$$\text{If } \beta, \kappa \text{ are independent of } T \Rightarrow P_2 - P_1 = \frac{\beta}{\kappa} (T_2 - T_1)$$

結果與 P2.9, (2.18) 的結果相同

實際上的 cooling 不可能是 reversible, 因加熱會造成系統內的溫度梯度。熱源與系統間亦有溫度梯度。

不過上述討論與 path 無關, 只與起點與終點有關。
故可任意選擇路徑, 方便上述 reversible process.

$$\text{That is, } \int_{P_1}^{P_2} dp = \frac{P}{K} \int_{T_1}^{T_2} dT$$

$$(P_2 - P_1) = \frac{P}{K} (T_2 - T_1) \quad \text{與路徑無關.}$$